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REVIEW ARTICLE

# Co-processed excipients with enhanced direct compression functionality for improved tableting performance

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## Abstract

It is necessary to have excipients with excellent functional properties to compensate for the poor mechanical properties and low aqueous solubility of the emerging active ingredients. Therefore, around 80% of the current drugs are not suitable for direct compression and more advanced excipients are required. Further, conventional grades of excipients cannot accommodate the technologically advanced high speed rotary tablet presses which require a powder with excellent flow, good compressibility, compactibility, particle size distribution and homogeneity of the ingredients. Co-processed excipients have been created to enhance the functional properties of the excipients and reduce their drawbacks. Co-processing is defined as the combination of two or more excipients by a physical process. Co-processed excipients are adequate for direct compression since they become multifunctional and thus, their dilution potential is high eliminating the need for many excipients in a formulation. In some cases, they are able to hold up to 50% of the drug in a formulation rendering compacts of good tableting properties. This study describes and discusses the functionality enhancement of commercial and investigational excipients through co-processing.

**Keywords:** Co-processed excipients, co-processing, direct compression, multifunctional excipients, particle engineering

## Enhancement of excipient functionality

Currently, the emerging new drugs in the market such as didanoside, lopinavir, podofilox, paclitaxel and oxaprocin exhibit physicochemical, solubility and pharmacokinetic properties, which challenge the requirements of the existing excipients during the drug product development phase. Further, the increasing speed capabilities of tablet machines are pushing excipient functionality to its limits. These problems require either the development of new excipients, or modification of commercial excipients. The pharmaceutical industry demands scientist develop excipients quickly, with limited scaling up, manufacturing and environmental costs. However, the search for new excipients requires extensive toxicology tests, which make them costly. For this reason, in the last three decades, new grades of existing excipients have been developed, but relatively few novel excipients have been introduced in the market<sup>1</sup>. An excipient is considered new when it contains a new chemical entity, is physically modified, is

a co-processed mixture of existing excipients, is directed toward a new route of administration, or when a food additive is used for the first time in a drug product<sup>2</sup>.

New grades of existing excipients can be achieved by modifying the powder fundamental properties leading to improved derived (functional) properties<sup>3,4</sup>. Fundamental characteristics, such as morphology, particle size, shape, surface area, porosity and density, determine excipient functional properties such as flowability, compressibility, compactibility, dilution potential, disintegration time and lubricant sensitivity (Figure 1).

Nevertheless, functionality can only be improved to a certain extent because of the limited range of possible modifications<sup>5</sup>. Powder density and particle size could be changed to achieve better functionality. However, when one attribute is improved, another is compromised. For example, the flow of Avicel® PH-200 is improved at the expense of its compactibility and vice versa for Avicel® PH-101<sup>6</sup>. Further, thermal treatment of native starches

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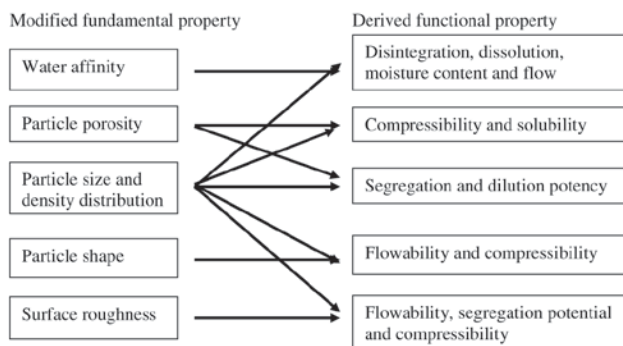


Figure 1. Effect of the material fundamental properties on the derived properties.

has led to an improved binder (pregelatinized starch). The starch granules are partially hydrolyzed and broken making them more hydrophilic<sup>7</sup>. This physical modification provides multiple functionality, such as excellent flow, self-lubrication property, filling application in hard gelatin capsules (5–75%), binding in wet granulation (5–20%), tablet disintegration functionality (5–10%), as well as roller compaction and direct compression applications<sup>8</sup>.

There are three levels of the solid state that can be modified to improve excipient functionality. These comprise the bulk, molecular and particle levels. The bulk level of a material can be modified by changing particle interaction in the bulk state<sup>5</sup>. This approach is widely used during the drug development stage and implies only a dry blend of two or more excipients in an exact ratio. The resulting blend will exhibit intermediate properties to those of the parent materials. In select cases, the magnitude of these properties is not ratio-dependent. Particle size, particle size distribution and bulk density of materials should be similar; otherwise, segregation will take place. Segregation may occur during manipulation, handling and storage of products rendering stability and batch to batch variability issues<sup>9</sup>. Thus, in the design and development of a product, it is not uncommon to use two or more excipients/coadjuvants to obtain a mixture with adequate tableting properties; the properties of such blends can result in either synergistic or antagonistic effect(s) with respect to various tableting properties<sup>6</sup>. For example, a dry blend can be used to formulate rapidly disintegrating tablets in which a mixture of Prosolv® SMCC, mannitol and a poorly soluble drug are compressed at low pressures and then freeze dried to make solid tablets. Prosolv® SMCC can absorb sufficient quantity of fine dust of fast dissolving excipients such as mannitol. The resulting compacts are able to disintegrate within 60 sec after contact with water or saliva<sup>10</sup>.

Similarly, mixtures of glyceryl dimenihate, a bitter drug, and microcrystalline cellulose (MCC) can be extruded-spheronized to form beads which are then coated with hydroxypropylmethylcellulose (HPMC) and compressed into tablets. These compacts disintegrate in the mouth within 20 sec<sup>11</sup>. In a few cases, the

API can be dispersed with the excipients and then spray-dried to form a more homogeneous blend. For example, acetaminophen can be spray-dried with maltodextrin to produce oblong free-flowing particles of good compactibility. In this case, the binary mixture has good compactibility, but the compacts show a capping tendency<sup>12</sup>. It may be necessary to diminish the deleterious effect of adjuvants in the bulk, which can, in some cases, be done simply by changing blending time. For example, the negative effect of magnesium stearate on plastic deforming materials can be reduced by decreasing the blending time to less than 5 min<sup>13</sup>.

The molecular level can be modified by changing the arrangement of molecules in the crystalline lattice, generating new allomorphs, pseudopolymorphs, making a material more amorphous or by applying a chemical treatment (crosslinking). Chemical modification of the material at a molecular level usually involves a crosslinking reaction between the excipient and a low molecular weight substance. This process is expensive and usually requires a solvent recovery technique. Furthermore, crosslinking agents are usually toxic and leave traces of by-products (impurities) that can degrade in living tissues to form toxic compounds. For example, MCC, starch, chitosan, lactose, and other sugars can be easily crosslinked with glutaraldehyde in a complex etherification reaction. However, glutaraldehyde also polymerizes, leading to the formation of undesirable by-products, which are difficult to remove<sup>14</sup>. There are several examples of widely used crosslinked excipients approved for pharmaceutical applications. For example, carboxymethylation of potato starch (ether synthesis), followed by neutralization with citric acid renders a superdisintegrant called sodium starch glycolate. Another type of starch crosslinking leads to a new product (hydroxyethyl starch) useful for parenteral applications. Further, cellulose derivatives such as ethyl cellulose (EC), methylcellulose (MC) and (HPMC) are other examples of chemically modified excipients<sup>15</sup>.

Modification of the crystalline structure also renders excipients with different properties. For example, microcrystalline cellulose I (MCCI) can be transformed to microcrystalline cellulose II (MCCII) by basic treatment. MCCII has a higher porosity, less packing tendency, degree of crystallinity, degree of polymerization and density, but a faster disintegration rate than MCCI. Further, compacts made of MCCII present better mechanical properties than those of MCCI<sup>16</sup>.

At the particle level, individual particles can be modified in shape, size, surface area and porosity by processing or co-processing with another inert material. Co-processing is based on the concept of excipient interaction at the subparticle level. It provides a synergy of functionality as well as masking the undesirable properties of the individual components<sup>3</sup>. Particles can be incorporated either on the surface, or within the core of the excipient particles. This process requires vigorous homogenization of the excipients, followed by a process such as spray drying, crystallization, spheronization,

bulk drying, etc. Co-processing is less expensive than crosslinking, as long as the materials involved comply with the pharmacopeia requirements because the toxicity studies required for a new material are not needed for co-processed products.

### Excipient co-processing

Co-processing is defined as a combination of two or more established excipients by a pharmaceutical process. The products so formed are physically modified such that they do not lose their chemical structure and stability. This means that excipients maintain their independent chemical properties; while, synergistically increase their functional performance<sup>17</sup>.

Usually, a co-processed material exhibits superior properties than the physical mixture of individual components. Ideally, a combination of a plastic and a brittle deforming material is desired for co-processing<sup>5</sup>. This combination prevents storage of too much elastic energy during compression, which is associated with the compacts tendency for capping and lamination<sup>18</sup>.

A major limitation of a co-processed excipient is that the ratio of the excipients in the mixture is fixed and while developing a new formulation, a fixed ratio of the excipients may not be desirable for the dose and characteristics of the API<sup>19</sup>.

Spray-drying, wet granulation, spheronization, co-milling, and co-crystallization can be used for co-processing. Spray-drying is a process in which an aqueous or organic dispersion of the materials is sprayed through a nozzle at high pressure, and the droplets formed are rapidly dried and collected as powder. Wet granulation involves the addition of an aqueous dispersion of a binder to a previously mixed powder blend followed by wet sieving and drying. In the spheronization process, first, the wet mixture of excipient(s) is extruded to produce homogeneous spaghetti-like rods. This extrudate is then converted to beads by using a spheronizer. Co-milling is used to disperse, homogenize and reduce the particle size of excipient mixtures in an aqueous media. In co-crystallization, the two materials are dissolved by heating, followed by cooling at different rates.

### Co-processed excipients

The main commercial and investigational co-processed excipients are summarized in Tables 1 and 2.

#### Lactose–Lactitol (Pharmatose®)

It is produced by spray drying of a 95% anhydrous  $\beta$ -lactose and 5% anhydrous lactitol solution. It is available in different grades depending on the particle size<sup>20</sup>. For example, the grade 100M has a median particle size of  $\sim 122 \mu\text{m}$  and a high density (bulk density of  $0.73 \text{ g/cm}^3$  and tap density of  $90 \text{ g/cm}^3$ ), which are responsible for its good flowability (Carr's index of 16%<sup>21</sup>). Low particle size grades ( $<32 \mu\text{m}$ ) are mainly used for nasal powder formulations<sup>22</sup>. Compacts made at 16 kN with diazepam showed disintegration times of 85 sec. It also possesses

a low water uptake (5.5%) at a relative humidity (RH) of 70%<sup>23,24</sup>.

#### Lactose–Cellulose (Cellactose®)

It is composed of 75%  $\alpha$ -lactose monohydrate and 25% powder cellulose obtained by spray drying. The good compactibility (tensile strength of 3.8 MPa at a solid fraction of 0.9) of this material is attributed to the synergic effect of consolidation by fragmentation of lactose and the plastic deformation of cellulose<sup>25</sup>. During spray drying, lactose particles coat the cellulose fibers forming granules of good flow. This excipient combines the good flowability and solubility of lactose with the good water sorption and binding properties of cellulose (tensile strength of 3.8 MPa at a solid fraction of 0.9<sup>26</sup>). It has a bulk density of  $\sim 0.38 \text{ g/cm}^3$  and a volume-diameter particle size of  $\sim 238 \mu\text{m}$ . It exhibits higher tensile strength than lactose (3.8 MPa vs. 1.8 MPa) and the dry blend of 75% lactose and 25% cellulose (2.0 MPa, respectively). It possesses better compressibility compared to Ludipress® (co-processed lactose monohydrate, povidone and crospovidone), Fast Flo 316® (spray-dried  $\alpha$ -lactose monohydrate), Tablettose® (spray-dried  $\alpha$ -lactose monohydrate), Dipac® (co-processed sucrose and maltodextrin) and anhydrous lactose. It also shows superior flow than Avicel® PH-101 (Carr's index of 22% and 34%, respectively<sup>27</sup>).

This material is virtually not affected by lubricants. During compaction, at low compression pressures, the fragmenting behavior predominates as many new surfaces of lactose are generated under compression and therefore, the lubricant sensitivity is low. However, at pressures higher than 180 MPa, plastic deformation given by the MCC component is prevalent since the outer lactose coating has already undergone fragmentation for both, the lubricated and non unlubricated materials. It has higher tensile strength than the physical mixture because of favorable interactions between lactose and MCC particles. It is also less sensitive to magnesium stearate than the physical mixture of 75% lactose and 25% MCC. Both, Cellactose® and the physical mixture exhibit an increase in tablet relaxation at high compression speeds<sup>25</sup>. Disintegration is slow and pressure-dependant, since it requires the lactose outer shell to dissolve and the resulting viscous layer recedes allowing access to the cellulose core. For example, compacts made at a compression pressure of 160 MPa, have a disintegration time of  $\sim 14 \text{ min}$ , whereas compacts made at 100 MPa have a disintegration time of 80 sec<sup>28</sup>. Further, compacts of made of Cellactose® at 150 MPa have comparable hardness (130–140 N), disintegration time (50–80 sec) and lower ejection forces (0.11 kN vs. 0.30 kN) than StarLac®<sup>23</sup>.

#### Lactose–MCC (Microcelac 100®)

It is a spray-dried material intended for direct compression composed of 25% MCC and 75%  $\alpha$ -lactose monohydrate. It has a median particle size of  $\sim 150 \mu\text{m}$ , superior

Table 1. Starch-based and cellulose-based co-processed excipients.

Type	Brand name	Manufacturer	Ingredients	%	Processing
Starch-based	Advantose® FS	SPI Pharma	Fructose	95	Spray-drying
			Starch	5	
	StarCap® 1500	Colorcon	Corn starch	90	Spray-drying
Cellulose based	a	10	Pregelatinized starch	10	cocrystallization
			Starch	50	
	Avicel® HFE	FMC	MCC	90	Spray-drying
			Mannitol	10	
	Avicel® RC-591	FMC	MCC	89	Milling, Spray-drying
			Na CMC	11	
	Avicel® RC-581	FMC	MCC	89	Milling, Bulk drying
			Na CMC	11	
	Avicel® CL-611	FMC	MCC	85	Milling, Spray-drying
			Na CMC	15	
	Avicel® HFE	FMC	MCC	90	Spray-drying
			Mannitol	10	
	Avicel® RC-591	FMC	MCC	89	Milling, Spray-drying
			Na CMC	11	
	Avicel® RC-581	FMC	MCC	89	Milling, Bulk drying
			Na CMC	11	
	Avicel® CL-611	FMC	MCC	85	Milling, Spray-drying
			Na CMC	15	
	Avicel® CE15	FMC	MCC	85	Spray-drying
Guar gum			15		
Barcroft® CS90	SPI Pharma	Calcium carbonate	90	Spray-drying	
		Starch	10		
ForMaxx®	Merck/EMD	Calcium carbonate	70	Spray-drying	
		Sorbitol	30		
ProSolv® SMCC50	JRS Pharma	MCC	98	Spray-drying	
		Colloidal silicon dioxide	2		
ProSolv SMCC90®	JRS Pharma	MCC	98	Spray-drying	
		Colloidal silicon dioxide	2		
Xylitab®200	Danisco	Xylitol	98	Granulation	
		Na CMC	2		
a	44,45	MCC	80	Spray-drying	
		Calcium carbonate	20		
a	97,98	MCCII	95	Spray-drying	
		Colloidal silicon dioxide	5		
a	64	Rice starch	70	Spray-drying	
		MCC	30		

<sup>a</sup> Under research

flowability and binding properties compared to the physical mixture of MCC with different lactose grades, such as  $\alpha$ -lactose monohydrate, anhydrous  $\beta$ -lactose and spray-dried lactose<sup>23,29</sup>. At compression forces between 6 and 8 kN the strength of its compacts is higher than that of Cellactose® with and without the addition of magnesium stearate. Compacts made at 6 kN disintegrate much faster than those made with Cellactose®80. Further, compacts made with ascorbic acid and Microcellac® possess higher strength than the ones made with Cellactose®80<sup>30</sup>.

#### Lactose–PVP (Ludipress®)

It consists of 93.4%  $\alpha$ -lactose monohydrate (filler), 3.2% Kollidon®30 (binder) polyvinyl pyrrolidone, ( $M_v$  44–54

kD) and 3.4% Kollidon®CL (disintegrant). It is produced by coating lactose with Kollidon®30 and Kollidon®CL<sup>27</sup>. It has good flow (Hausner ratio of 1.2) due to the predominant spherically-shaped particles, which contain a large number of small lactose crystals with smooth surfaces held together by Kollidon®30 and Kollidon®CL<sup>27</sup>. It has a bulk density from 0.50 to 0.57 g/cm<sup>3</sup>. It requires magnesium stearate for lubrication since it develops friction during compression. However, magnesium stearate increases tablet friability and disintegration times. Compacts made at >100 MPa show friability values lower than 1%<sup>13</sup>. Its volume-diameter particle size is ~210  $\mu$ m. Although it contains disintegrant, disintegration of the tablets takes longer than those containing

Table 2. Lactose-based, sugar-based and other co-processed excipients.

Type	Brand name	Manufacturer	Ingredients	%	Processing	
Lactose-based	Cellactose®	Meggle	$\alpha$ -Lactose monohydrate	75	Spray-drying	
			Powder cellulose	25		
	Ludipress®	27		$\alpha$ -Lactose monohydrate	93.4	Roller drying
				Crosspovidone	3.4	
				PVP	3.2	
				$\alpha$ -Lactose monohydrate	75	
Microcellac®	Meggle		MCC	25	Spray drying	
Pharmatose®DCL40	DMV Vengel		$\beta$ Lactose	95	Spray drying	
			anhydrous Lactitol	5		
StarLac®100	Meggle/Roquette		$\alpha$ -Lactose monohydrate	85	Spray drying	
			Corn starch	15		
Sugar-based	Di-Pac®	Domino Specialty Ingredient	Sucrose	97	co-crystallization	
	Compressol®S	SPI Pharma	Maltodextrins	3	Melt extrusion	
			Mannitol	70		
	F-Melt®	Fuji health Science		Sorbitol	30	Spray drying
				Xylitol, calcium hydrogen phosphate	40–90	
	LudiFlash®	BASF		Crospovidone	5–40	Granulation
				Mannitol	90	
				PVA latex solids	5	
	Sugar Tab®	JRS Pharma		Crospovidone	5	Crystallization
				Sucrose	93	
Xylitab®100	Danisco		Invert sugar	7	Granulation	
			Xylitol	96.5		
			Polydextrose	3.5		
			Sucrose	95		
a	78		Sorbitol	5	co-crystallization	
Others	Effer Soda®	SPI Pharma	Na carbonate	10	Spray coating	
	Timerx®	Penwest	Na bicarbonate	90	NR	
			Xanthan gum	NR		
	a	43		Locust bean gum		Codrying
				Chitosan	50	
				Silica	50	
	a	59		PVP	75	co-crystallization
a	86		Sodium starch glycolate	25	Hot melting	
			Wax	5		
			Calcium phosphate	95		

NR, Not reported; a, Under research.

$\alpha$ -lactose,  $\beta$ -lactose and spray-dried lactose alone, because of the presence of Kollidon® 30 in the excipient. For example, if compacts are made at 250 MPa, they disintegrate in ~4 min, whereas compacts made of Tablettose® and the physical blend take about 13 min and 1 min, respectively. It has a lower compactibility (160 N) than Cellactose® (180 N), but larger than that of Avicel® PH-200, Tablettose® and its physical blend (140 N, 90 N and 60 N, respectively<sup>27</sup>). It also shows a lower yield pressure than that of Avicel® PH-102 (86 vs 49 MPa, respectively) and it also has good tableting characteristics for low dose APIs such as glibenclimide (2 mg) and its hardness is not affected by tableting speed<sup>32</sup>. It also exhibits better flowability than Cellactose® Tablettose® and Avicel® PH-200 (angle of repose of 31°, 36°, 36° and 36°, respectively<sup>27,33</sup>).

#### Lactose–starch (StarLac®)

It is produced by spray-drying of 85% lactose monohydrate and 15% native maize starch. It is an adaptable excipient since the two materials alone present poor flow and segregation problems, which restrict them to use in the wet granulation process. Crystalline lactose monohydrate provides a good diluent capacity; whereas, native starch functions as a tablet disintegrant. It has a median particle size of ~55  $\mu$ m, bulk density of ~0.6 g/cm<sup>3</sup> and its particles exhibit a spherical shape. In this excipient, starch is dispersed within a matrix of predominantly crystalline  $\alpha$ -lactose monohydrate. It also exhibits excellent direct compression capability similar to that of spray-dried lactose. Tablets made between 40 and 120 kN show disintegration times within 23 sec<sup>34</sup>. Moreover, different levels of lubricants do not affect tablet disintegration time. This

means that tablets maintain their porosity and the presence of starch allows for rapid tablet disintegration, irrespective of the tablet hardness, eliminating the need of a super disintegrant<sup>35</sup>. It also has excellent flow due to the uniform particle size and hence, presents little risk of segregation. It does not have a gritty taste, provides a creamy texture in the mouth, and therefore, is appropriate for use in soft chewable tablets applications. It does not cross-link with gelatin capsule shells and hence, does not delay disintegration. StarLac® is better for roller compaction than MCC since it generates less dust during milling of the resulting ribbons. It also has higher compressibility and less elastic recovery than MCC<sup>3</sup>. At high relative densities, compact elastic recovery and disintegration time are lower, compactibility is higher and, compared to the physical mixture of the individual components. StarLac® produces tablets with lower crushing strength than tablets made using the physical mixture containing 0.5% magnesium stearate. However, for the physical mixtures, disintegration time increases with increasing levels of magnesium stearate<sup>36</sup>. Compared with other co-processed excipients, the lubricant sensitivity to magnesium stearate varies as: StarLac®>Ludipress®>Cellacose®80>Microcellac®100. The elasticity of StarLac® is influenced at low compression forces by lactose and at high compression forces by starch<sup>34</sup>.

#### **Starch–fructose (Advantose FS®95)**

This material is produced by spray drying of 95% fructose and 5% starch. This excipient overcomes the poor dissolution and compactable properties of fructose alone. It is ideal to formulate chewable vitamins. It is a white crystalline powder of a porous granular shape and rough surface<sup>37,38</sup>. It has a moisture content of ~2%, a bulk density between 0.55 and 0.75 g/cm<sup>3</sup> and a mean particle size of ~ 300 µm. It also has good flow and compressibility. It is less hygroscopic, and easier to handle than fructose, and it is more compactable than Dipac®<sup>39</sup>.

#### **Starch–pregelatinized starch (StarCap®1500)**

This is a co-processed mixture of corn starch and pregelatinized starch for use in capsule applications. It is an inert, free-flowing, low dust excipient with disintegration and dissolution properties independent of the medium pH. It has better flow properties than MCC. It allows for minimal dusting or adherence to contact surfaces, leading to a cleaner filling operation and lower tablet weight variation. StarCap® at >75% level makes the release profile of propranolol pH-independent and at a 24.75% level allows for the release of 90% of gabapentin within 6 min<sup>40</sup>. Other studies suggest StarCap® 1500 to have better compressibility, shorter disintegration time, higher lubricant sensitivity and lower elastic component of energy comparison to Starch® 1500<sup>41</sup>.

#### **Starch–silica (50:50)**

This excipient is prepared by adding SiO<sub>2</sub> to a 4% dispersion of corn starch at 100°C. After the dispersion is

cooled down, the addition of ethanol causes precipitation and thus, the particles are collected by filtration. Co-processing resulted in a crystalline form of starch within the amorphous SiO<sub>2</sub> matrix. The co-precipitate has a surface area between ~15 m<sup>2</sup>/g vs 200 m<sup>2</sup>/g of SiO<sub>2</sub> and 0.28 m<sup>2</sup>/g for starch, respectively<sup>42</sup>. It has a good flow (Carr's index ~12%), tensile strength (3.0 MPa) and compressibility. Tablets of this excipient show better disintegration time (5 sec) than the one produced from starch (5 min), sodium starch glycolate (10 min), and croscarmellose (10 min). This excipient was designed as superdisintegrant and it alone renders a disintegration time of less than 10 sec for tablets compressed at 50 kN. It produces granules with good strength when hydroxypropyl cellulose is used as a binder<sup>43</sup>.

#### **MCC–Calcium carbonate (80:20)**

This co-processed excipient is composed of 80% MCC and 20% CaCO<sub>3</sub>, prepared by spray drying. The CaCO<sub>3</sub> component provides a more uniform surface, giving a smooth appearance to the tablets. The particle size ranges from 20 to 150 µm. Ground limestone and MCC have bulk densities of 0.67 g/cm<sup>3</sup> and 0.29 g/cm<sup>3</sup>, respectively; whereas, the co-processed product has a bulk density of 0.41 g/cm<sup>3</sup>. The increased bulk density of the co-processed product allows for making smaller tablets and improved powder flow into the dies. Its aqueous slurry has a pH between 9.5 and 10. It also contains low moisture content (<8%). This co-processed excipient is useful to load drugs with bulk density lower than 0.30 g/cc<sup>44,45</sup>. The co-processed product exhibits low lubricant sensitivity and its compressibility is high even at high levels of API.

#### **MCC–guar gum (Avicel® CE15)**

This material is produced by spray drying of a dispersion made of 85% MCC and 15% guar gum. It has a nominal particle size of 75 µm. The presence of guar gum decreases the chalkiness, grittiness, and taste caused by MCC. The presence of guar gum makes it suitable to formulate chewable compacts<sup>45–47</sup>. Compared to MCC:NaCMC, Avicel®CE15 granules made by roller compaction renders granules of poor compactibility<sup>48</sup>.

#### **MCC–mannitol (Avicel®HFE)**

This co-processed excipient is produced by spray drying a mixture of 90% MCC and 10% mannitol. The bulk density of the co-processed product is ~0.4 g/cm<sup>3</sup>. The MCC component imparts greater compressibility and compactibility to the composite particles, but it compromises flow. The mannitol component provides good mouth-feel (due to its negative heat of solution), low grittiness, low chalkiness, low sensitivity to humidity, low plasticity and high dissolution rate (due to its high aqueous solubility and wetting properties). As a result, the co-processed product has excellent compressibility, good water wicking, and good water absorption capacity. The co-processed material provides good powder and compressibility properties with disintegration times within 15 sec. Mannitol crystals

are uniformly distributed within the MCC matrix, as opposed to the physical mixture. It has been reported that the fast compact disintegration is due to the partial amorphization and formation of submicron particles of the soluble mannitol on the surface and within the MCC matrix by spray drying. This co-processed product has higher porosity than the physical mixture and this effect is reflected in the faster disintegration time of compacts made with glizipide (1.3 min vs. 4.1 min). This excipient is ideal for making fast dissolving tablets<sup>18</sup>. Compacts containing Avicel®HFE and acetaminophen are less friable and significantly more compactable than those containing MCC and mannitol alone<sup>49</sup>. However, they suffer from loss of compactibility after reprocessing. For example, the initial compact strength of 10 MPa is reduced to 6.2 MPa after further milling and recompression.<sup>50</sup>

#### **MCC–NaCMC (Avicel®RC591/RC581/Avicel®CL611)**

Avicels® RC591/581 are composed by 89% MCC and 11% sodium carboxymethylcellulose (NaCMC). Avicel® RC-591 is produced by spray drying of their aqueous slurry, while Avicel® RC-581 is produced by bulk drying of the slurry of both components. Avicel® CL-611 is produced by spray drying of an aqueous dispersion of 85% MCC and 15% sodium carboxymethylcellulose. Compacts made of Avicel® RC-581 and Avicel® PH-101 release ~77.1% and 38.9% of glizipide within 360 min, respectively<sup>51</sup>. Avicel® RC-591/RC-581/Avicel® CL-611 are dispersible celluloses used as suspending aids to improve the stability and texture of dispersed systems, like suspensions, emulsions, creams, lotions, etc. They produce a firm gel structure via steric stabilization due to particle interactions<sup>52,53</sup>. NaCMC is added to aid the dispersion and to serve as a protective colloid. As the proportion of CMC is increased to about 10% w/w in mixtures of MCC and CMC, gels are formed having a maximum yield stress, while a proportion of CMC exceeding 10% results in decreased values of yield stress. Avicel®RC-591 and Avicel® RC-581 are used from 1 to 2% for nasal sprays, topical sprays, lotions and oral suspensions. Avicel® CL-611 is mainly used for reconstitutable suspensions and oral suspensions<sup>54</sup>.

#### **MCC–SiO<sub>2</sub> (Prosolv®)**

Prosolv® is the spray-dried product of MCC and SiO<sub>2</sub> made at the 98:2 ratio. It is available in three grades: Prosoolv® SMCC90, Prosoolv® SMCC50 and Prosoolv® SMCC HD90 which corresponds to a mean particle size of 110 µm, 60 µm, and 110 µm, and a bulk density of ~0.30 g/cm<sup>3</sup>, 0.30 g/cm<sup>3</sup> and 0.44 g/cm<sup>3</sup>, respectively. Prosoolv® SMCC50 is recommended for direct compression of poorly compactable API and for roller compaction<sup>55</sup>. Prosoolv® SMCC90 is desirable to improve flow of the powder mixture and reduce the need for glidants. Prosoolv® SMCC HD90 which is produced from hardwood sources is suggested for formulations which require good flow, good consolidation and when denser compacts are needed. It has particles with a more spherical shape and

it is less tableting rate sensitive than Prosoolv®SMCC50 and Prosoolv®SMCC90. Prosoolv®SMCC90 has better flow and produces stronger compacts than Avicel®PH-200 (28 and 32°, and 170 N and 95 N, respectively). This represents a considerable increase in the binding capability of Prosoolv® and is responsible for the good “dilution potential” of this material<sup>56,57</sup>. Prosoolv® SMCC90 and Prosoolv® SMCC HD90 have low sensitivity to magnesium stearate (0.12 and 0.19, respectively). Silicon dioxide markedly suppresses the negative effect of stearate on the binding properties of MCC. This is explained by the interaction of silicon dioxide and magnesium stearate in the sense of competitive inhibition of stearate in the sites of adhesion, which are blocked by SiO<sub>2</sub>. The physical blend has no significant contribution on the tablet strength of lubricated and non-lubricated tablets. Dissolution rate and friability are similar to conventional MCC<sup>30,58</sup>. However, Prosoolv® compacts have poor disintegration properties (from 20 to 30 min for compacts compressed at 4kN)<sup>59</sup>. Further, the compactibility of Prosoolv® is slightly affected by wet granulation<sup>60</sup>. The above mentioned properties are due to the uniform adhesion of SiO<sub>2</sub> to the surface of MCC. The increased compact strength is most likely a consequence of surface interaction between SiO<sub>2</sub> and MCC<sup>61</sup>. SiO<sub>2</sub> interacts with cellulose possibly through hydrogen bonding and dipole-dipole interactions and thus, SiO<sub>2</sub> leads to a five-fold surface increase compared to MCC<sup>62,58</sup>. Further, SMCC has also been reported to decrease the lower punches stickiness compared to the physical mixture of MCC and SiO<sub>2</sub><sup>62</sup>.

For developing orally disintegrating compacts, Prosoolv® cannot comprise > 30% level in the compact because it leaves an unpleasant gritty sensation in the mouth and it does not dissolve in saliva. Prosoolv® possess a high degree of surface roughness, which increases powder shear in the dry blending process and ease low dose API loading. Prosoolv®, also might prevent oxidation of some APIs (i.e., iron and levothyroxine). It is also good for tacky or cohesive APIs and retains high compactibility after reworking<sup>63</sup>.

#### **MCC–Rice starch**

This is produced by spray drying of 70% rice starch and 30% MCC. The use of starch as the major component in the composite is preferred because of the abundance of inexpensive rice starch. The cellulose component imparts greater compressibility to the composite particles, but makes particles less spherical, with rougher surfaces, resulting in a decrease in flowability. Among several native starches, rice starch is the most compressible, but the flowability of rice starch is very poor because of the small size range of starch grains. During spray drying, the heat could induce partial gelatinization of the surface of the starch grains. Gelatinization of starch grains might be responsible for binding rice grains and cellulose fibers together through solid bridge forming granular particles. Spray drying affects particle shape, but not the compactibility of rice starch. Compacts made of this material show good compactibility (~189 N), low friability



(0.6 %), good flow (Carr's index of 19.2%) and disintegration properties (2.6min), compared to rice starch (131 N, 0.6%, 44.6% and 1.9min, respectively) and MCC (490 N, 0.0%, 38%, and >30min, respectively<sup>64</sup>).

#### **Dextrose–Maltose–Maltodextrin (Emdex®)**

This commercial material is produced by spray drying a solution composed of 92% dextrose, 4% maltose and 4% maltodextrin. Emdex® is 74% as sweet as sucrose and it is composed of porous spheres<sup>65</sup>. It has good flow, compressibility, lubricity, non-hygroscopicity, controlled particle size, cool mouth-feel, negative heat of solution, and stability to heat and moisture, making it useful for direct compression of lozenges and chewable soluble compacts. The spherical porous granules consist of flat microcrystals bound together by higher saccharides<sup>66</sup>. It is reported that compacts produced from Emdex® using the direct compression method showed low elastic work (6 J) and ejection forces (0.8 kN), requiring less lubrication than compacts produced by wet granulation (elastic work of 1.6 kN and ejection force of 12 kN, respectively). Similarly, if used for wet granulation, it decreased the crushing force of the tablets and enhanced lubrication, compared to direct compression formulations. The Heckel analysis shows that this material exhibits a plastic deformation mechanism<sup>67</sup>.

#### **Mannitol–Kollidon (LudiFlash®)**

It is a co-processed product intended for use as an excipient for orally disintegrating tablets. It is composed of 90% mannitol, 5% Kollidon® and 5% polyvinyl acetate. It possesses rapid dissolution, smooth mouth feeling and excellent compressibility<sup>31</sup>. It has a bulk and tap densities of 0.45 and 0.55 g/cm<sup>3</sup>, respectively, and a mean particle size and moisture content (MC) of ~190 µm and ~4%, respectively. It imparts no chalky or sandy sensation, but a creamy consistency. It exhibits high swelling in contact with water and saliva. Tablets made at 10 kN pressure exhibit good hardness (120 kN), low friability (0.12%), and low ejection forces (50 kN). It can be used for direct compression, wet granulation or roller compaction. It serves as a filler, a binder and a disintegrant all-in-one. It requires low lubricant levels for tableting and has no segregation tendency. Compacts made of LudiFlash® and loperamide at 3.7 kN have a hardness of 30 N, disintegration time of 11 sec and drug release of 95% within 30 min<sup>68,69</sup>.

#### **Mannitol–Sorbitol (Compressol®S)**

It is a co-processed excipient made up of 70% mannitol (a low hygroscopic material with a pleasant sweet taste) and 30% sorbitol (a highly compactable and very hygroscopic material). It is produced by melt extrusion. It has a volume-diameter of ~360 µm. It is 300% less hygroscopic than sorbitol and a moisture content <1%. This material does not have the sticking problem of sorbitol during tableting. It is suitable for development of orally disintegrating compacts of moisture sensitive drugs, as well as

for lozenges and chewable compacts. For example, tablets made of ascorbic acid and Compressol® disintegrate within 70 sec; whereas, those made with glucosamine (high dose drug) disintegrate within 130 sec. At 30 kN compression force compacts of mannitol have a crushing force of ~15 kP and those of Compressol® of ~35 kP<sup>70</sup>.

#### **Sucrose–Invert Sugar (Sugartab®)**

It is a white, crystalline, odorless and free flowing, powder used for direct compression of tablets. It is produced by co-crystallization of 93% sucrose and 7% invert sugar. It is a white granular powder having an average particle size of 300 µm. It has a tap density of 0.7 g/cm<sup>3</sup> and a moisture content of 1%<sup>71</sup>. It has the same sweetness value as sucrose. It is sweeter than Emdex®, and it is able to produce zinc acetate lozenges with good taste. When blended with the active ingredient and a suitable lubricant, direct compression produces non-friable tablets with moderate hardness. This excipient has a poor flow (angle of repose of 36°), moderate compactibility (hardness/friability ratio of 3.4), and taste-masking characteristics. Further, it has a low hygroscopicity, good chemical stability, and gradual disintegration (~12 min). Avicel®PH-101 has an angle of repose of 48°, a hardness/friability ratio of 8.8 and a disintegration time of 75 min<sup>72</sup>. It has been used in the development of vitamin formulations, which might have compression problems. However, scientists reported that it is not the best excipient for formulating vitamin B1<sup>73</sup>.

#### **Sucrose–Maltodextrin (Di-Pac®)**

It is a co-crystallized product made by combining 97% sucrose and 3% maltodextrin. It is a white, crystalline, soluble powder of high flowability (angle of repose of 49°), high bulk density (0.66 g/cm<sup>3</sup>), hygroscopicity, low MC (0.5%) and good sweetness. It consolidates into a tablet by both, brittle and plastic deforming mechanisms, attributed by the sucrose and maltodextrin components, respectively. This excipient overcomes the poor compression properties of sucrose. It has a mean particle size of ~280 µm<sup>74–76</sup>. Granules are composed of hundreds of sucrose crystals entrapped within a maltodextrin matrix exhibiting a porous structure and a large surface area. It has excellent color stability on aging and its dilution potential ranges from 20 to 35%<sup>77</sup>. It flows better when the moisture content is from 0.4 to 0.8%. However, it requires a glidant if stored at (RH) >50%. High relative humidities have a negative effect on compactibility. For instance, its compacts harden hours after manufactured, or if stored at high RH followed by storage at low RH. This behavior is typical for sucrose<sup>49</sup>.

#### **Sucrose–Sorbitol**

It is a free flowing compressible sucrose with a pleasant taste, consisting of 95% sucrose and 5% sorbitol obtained by co-crystallization. The new directly compressible sucrose absorbs three times more oil than sucrose and 2.5 times more oil than the dry blend of sucrose and

sorbitol. This material renders stronger tablets than the individual components. Its compressibility can be attributed to the small sorbitol component, since sorbitol itself compresses into a very strong tablet. Sucrose-sorbitol tablets disintegrate quickly regardless of the tablet hardness. This compressible sucrose disintegrates and dissolves quickly, in ~30 sec, due to the porous and open crystalline structure of the excipient. Since sucrose has a high heat of fusion (126.6 J/g) and strong sweet taste, this excipient is useful to mask the bitter taste of active ingredients, leaving a cool sensation in the mouth<sup>78,79</sup>.

#### ***Xylitol–Dextrose (Xylitab®100)/Xylitol–NaCMC (Xylitab®200)***

They are produced by granulation of 96.5% xylitol and 3.5% polydextrose, and 98% xylitol and 2% sodium carboxymethyl cellulose for Xylitab®100 and Xylitab®200, respectively. Xylitabs® have a cool taste and good physical and chemical stabilities. Morris and collaborators<sup>80</sup> found compaction profiles, flow behavior and dilution potential of Xylitabs® as acceptable. They have been successfully utilized as a chewable tablet excipient for direct compression<sup>81</sup>. Compacts made of Xylitab®100 possess higher tensile strength, but more sensitivity to magnesium stearate than compacts of Xylitab®200. Disintegration time is longer for compacts made of Xylitab®200 than those containing Xylitab®100. Disintegration time is also delayed in presence of lubricants<sup>82</sup>.

#### ***Xylitol–Crospovidone–Calcium hydrogen phosphate (F-Melt®)***

It is a spray-dried product composed of xylitol (40–90%), crospovidone (5–40%) and calcium hydrogen phosphate (1–30%). The actual composition of the excipient can be changed, rendering two grades designated as C and M, where C is used for fast disintegrating excipients and type M for excipients that show better flow and compactibility. It is comprised of porous spherical particles of bulk density from 0.53 to 0.6 g/cm<sup>3</sup> and a mean particle size from 100 to 130 µm. It is non-hygroscopic since it only adsorbs 5% water at 75% RH. This excipient provides a good mouth-feel, stability, flow, tablet hardness, low friability and high API loading. It does not cause sticking or capping problems. It is designed for manufacturing oral disintegrating tablets (ODTs). Usually these ODTs have *in vitro* disintegration time of ~30 seconds. It is usually employed at a level ranging from 10 to 65% in a drug formulation. For instance, compacts made using 30% acetaminophen, 64.6% F-Melt, 5% crospovidone and 0.4% magnesium stearate have a disintegration time of ~12 sec and a hardness of ~53 N<sup>83</sup>.

#### ***Calcium Carbonate–Sorbitol (ForMaxx®)***

This co-processed excipient is composed of 70% calcium carbonate and 30% sorbitol prepared by spray drying. It has a bulk density of 0.7 g/cm<sup>3</sup> and moisture content of <1%. This material is highly compressible, possesses excellent taste-masking effect and free flowing properties, rendering superior drug content uniformity than the individual components and the physical blend. For

example, compacts made at 20 kN have a hardness of 300 kN and ~40 kN for ForMaxx® and the physical mixture, respectively. It is used for formulating antacids, calcium supplements, and its compacts show low friability. Sorbitol also masks the chalkiness and gritty taste of calcium carbonate<sup>5,84</sup>.

#### ***Chitosan–silica***

This excipient is produced by co-precipitation of 50% chitosan and 50% silica. SiO<sub>2</sub> is incorporated via partial coating, without any evidence of chemical interaction between the two ingredients. SiO<sub>2</sub> is responsible for increasing the bulk and tap densities giving better flowability and a more fragmenting behavior to the composite material. It has a high bulk density (0.5 g/cm<sup>3</sup>) and good flow (Carr's index of 10%). This excipient is water insoluble and non-hygroscopic at RH lower than 76%, but is able to accelerate compact disintegration upon contact with water. It has superior water uptake, disintegration characteristics with improved powder flow and compaction properties than the physical mixture of chitosan and silica. It also exhibits superior performance in wet granulation formulations than the physical blend. This excipient could act as disintegrant and pharmaceutical filler at the same time. Compacts made at 30 kN show a hardness of 55 N and a disintegration time of less than 5 sec<sup>43,85</sup>.

#### ***C–Crospovidone:sodium starch glycolate***

The co-crystallized disintegrant is composed of 75% crospovidone (Polyplasdone-XL10) and 25% sodium starch glycolate. The two materials are dissolved in isopropyl alcohol at 65°C and then stirred until most of the isopropyl alcohol is evaporated. The wet mass is then passed through a 60 mesh sieve and tray-dried at 60°C for 20 min. Polyplasdone® XL10 exhibits good compressibility and a high rate and extent of water uptake irrespective of the medium pH. On the other hand, sodium starch glycolate (SSG) has good hydration and swelling capacity and its disintegration ability is not affected by hydrophobic lubricants. In general, the composite disintegrant is used from 4 to 66%. Since, the bulk density of both materials is very different (0.40 vs. 0.76 g/cm<sup>3</sup>, respectively), the physical mixture is not suggested to use because of the inherent risk of segregation. Interestingly, compacts made of the physical blend showed higher crushing strength than tablets made of the co-processed disintegrant. However, compacts of both physical blend and co-processed products disintegrate within 4 min. If SiO<sub>2</sub> is added to the co-processed disintegrant, the tensile strength is virtually unchanged. Compacts made of Cefixime trihydrate presented a disintegration time of ~170 sec and release of 72% of the drug after 5 min. However, ibuprofen formulations with the disintegrant had a hardness of 6 N and disintegration time of 0.45 min, whereas, if croscarmellose sodium is used, compact hardness is 50 N, and disintegration time of 8 min. Further, if crospovidone is used compact hardness is 100 N, and disintegration time of 10 min<sup>33,86</sup>.

**Wax–calcium diphosphate**

It is composed of 5% fatty acid wax and 95% calcium diphosphate. It can be produced by hot melting using a high shear granulator, or by extrusion of the hot mass under vacuum or nitrogen. The resulting particle size ranges between 75 and 200  $\mu\text{m}$ . Calcium phosphate alone is abrasive and triggers lamination and capping in the compacts, especially at high compression pressures. This effect is exacerbated by the use of concave tooling. It is incompatible with pH sensitive active ingredients since the surface of milled anhydrous calcium phosphate is alkaline. Wax delays the disintegration time and decreases compressibility of calcium phosphate. Wax alone has poor flow properties due to its large particle size and interparticle adhesion. The acidic nature of wax also reduces the pH of calcium phosphate<sup>87</sup>. This co-processed excipient has a higher bulk density (0.76–0.86 g/cm<sup>3</sup>), porosity (70%) and abrasion tendency than calcium phosphate (bulk density and porosity of 0.66–0.71 g/cm<sup>3</sup> and 64%, respectively) and at the same time overcomes the poor flow characteristic of the wax, leading to a good content uniformity and minimization of segregation. Tablets made from this composite erode slowly since the hydrophobicity of the excipient reduces the accessibility to water, including gastric and intestinal fluids. Compacts made of this excipient and venlafaxime releases about 75% of this API after 2 h<sup>87</sup>.

**Xanthan–locust bean gum–dextrose (Timerx®)**

It is a co-processed product made from the bacterial polysaccharide named xanthan gum, a plant polysaccharide (locus bean gum), and dextrose at different ratios, which determine the release profile. By changing these ratios the release profiles of the API could be zero, first or second order<sup>88,89</sup>. Thus, it can be used to develop formulations from insoluble to highly-soluble drugs, at different doses<sup>90</sup>. Tobyn and collaborators found that high shear mixer granulation was superior to fluid bed granulation to produce granules of high density, mean particle size and flow (0.53 g/cm<sup>3</sup>, 380.5  $\mu\text{m}$  and 9.86 g/sec) on mixtures containing 25% xanthan gum, 25% locust bean gum and 50% dextrose<sup>91,92</sup>. Compacts made from the mix shear granules were stronger than the ones produced by fluid bed granules (crushing strength of 0.89 MPa and 1.51 MPa, respectively)<sup>93</sup>.

**Microcrystalline cellulose II: Silicon dioxide (95:5)**

A Cellulose II-based microcrystalline cellulose was introduced as a new direct compression excipient<sup>94–96</sup>. It is produced by mercerization of MCCI in an aqueous sodium hydroxide solution (>5N)<sup>97</sup>. MCCII is less ductile than MCCI, and its compacts, irrespective of the compression force used to prepare them, show rapid disintegration (within 30 sec). A new co-processed product was formed by spray drying of MCCII and SiO<sub>2</sub> at the 95:5 ratio. This material produced compacts of superior mechanical properties than MCCII alone, but comparable to those of Avicel® PH-102 and preserved the fast

disintegrating properties of MCCII<sup>98</sup>. It also showed a high specific surface area, a very low sensitivity to magnesium stearate, good flow, dilution ability and a more brittle deforming ability than MCCII. These properties result from the physical interaction of fumed silica when coating MCCII particles<sup>99</sup>.

**Conclusions**

The pharmaceutical industry has been forced in recent years to search for excipients with improved functionality due to the high demands for productivity. The most economical, simple and efficient approach to improve particle engineering has been through co-processing of two or three conventional excipients. These multifunctional excipients are usually employed for direct compression due to the improved functionality respect to the parent materials and their mere physical blending. In most cases, properties such as flowability, compactibility, dilution ability, and compressibility are enhanced with co-processing.

**Declaration of interest**

The authors report no conflicts of interest.

**References**

1. Chang D, Chang R. (2007). Review of current issues in pharmaceutical excipients. *Pharm Technol*, 31:1–2
2. Larner G, Schoneker D, Sheehan C, Uppoor R, Walsh P, Wiens R. (2006). Pharmaceutical excipient testing and control strategies. *Pharm Technol*, 1:1–7.
3. Block LH, Moreton RC, Apte SP, Wendt RH, Munson EJ, Creekmore JR, Persaud IV, Sheehan C, Wang H. (2009). Co-processed excipients. *Pharm Forum*, 35:1026–1028.
4. Reimerdes D. (1993). The near future of tablet excipients. *Manuf Chem*, 64:14–15.
5. Nachaegari SK, Bansal, AK. (2004). Co-processed excipients for solid dosage forms. *Pharm Technol*, 28:52–65.
6. Lerk C, Bolhuis G, De Boer A. (1974). Comparative evaluation of excipients for direct compression, II. *Pharm Weekbl*, 109:945–955.
7. Klinger R, Meuser F, Niediek E. (1986). Depolymerization of starch by high pressure extrusion. *Starch/Starke*, 38:40–44.
8. Ashish A, Neves S. (2006). From commodities to specialized excipients. *Phar Health News*, 4:5–8.
9. Levin M. (2006). Wet granulation: End-point determination and scale-up. *encyclopedia of pharmaceutical technology*. New York: Marcel Dekker, 4078–4098.
10. Beso A, Sirca J, Inventors. (2006). Rapidly disintegrating orodispersible composition containing non filamentous co-processed polyols particles and silicified microcrystalline cellulose. EP 1773292.
11. Burjak M, Legen I, Kerc J, Inventors. (2008). Orally disintegrating tablets. WO/2008/077813.
12. Gonnissen Y, Gonçalves SI, Remon JP, Vervaet C. (2008). Mixture design applied to optimize a directly compressible powder produced via cospray drying. *Drug Dev Ind Pharm*, 34:248–257.
13. Jivraj I, Martini LG, Thomson CM. (2000). An overview of the different excipients useful for the direct compression of tablets. *Pharm Sci Technol Today*, 3:58–63.
14. Rasmussen KE, Albrechtsen J. (1974). Glutaraldehyde. The influence of pH, temperature, and buffering on the polymerization rate. *Histochem Cell Biol*, 38:19–26.

15. Krassig H., editor. (1996). *Cellulose, Structure, Accessibility and Reactivity*. Amsterdam: Gordon and Breach science publishers. pp. 371
16. Rojas J, López A, Gamboa Y, González C, Montoya F. (2011). Assessment of processing and polymorphic form effect on the powder and tableting properties of microcrystalline celluloses I and II. *Chem Pharm Bull*, 59:603-607.
17. Chow K, Tong HH, Lum S, Chow AH. (2008). Engineering of pharmaceutical materials: An industrial perspective. *J Pharm Sci*, 97:2855-2877.
18. Jacob S, Shirwaikar A, Joseph A, Srinivasan K. (2007). Novel co-processed excipients of mannitol and microcrystalline cellulose for preparing fast dissolving tablets of glipizide. *Indian J Pharm Sci*, 69:633-639.
19. Saha S, Shahiwala AF. (2009). Multifunctional co-processed excipients for improved tableting performance. *Expert Opin Drug Deliv*, 6:197-208.
20. Bolhuis G, Zuurman K. (1995). Tableting properties of experimental and commercially available lactose granulations for direct compression. *Drug Dev Ind Pharm*, 21:2057-2071.
21. Atassi F, Almaya A, Aburub A. (2008). Effect of storage conditions on compaction behavior of two grades of spray-dried lactose. *Pharm Dev Technol*, 13:277-282.
22. Steckel H, Bolzen N. (2004). Alternative sugars as potential carriers for dry powder inhalations. *Int J Pharm*, 270:297-306.
23. Sebathu T, Elamin AA, Ahlnek C. (1994). Effect of sorption on tableting characteristics of spray-dried (15% amorphous) lactose. *Pharm Res*, 11:1233-1238.
24. Stubberud L, Arwidsson HG, Hjortsberg V, Graffner C. (1996). Water-solid interactions. III. Effect of glass transition temperature, T<sub>g</sub>, and processing on tensile strength of compacts of lactose and lactose/polyvinyl pyrrolidone. *Pharm Dev Technol*, 1:195-204.
25. Arida AI, Al-Tabakha MM. (2008). Cellactose a co-processed excipient: A comparison study. *Pharm Dev Technol*, 13: 165-175.
26. Belda P, Mielck J. (1996). Tableting behavior of cellactose compared with mixtures of celluloses with lactoses. *Eur J Pharm Biopharm*, 42:325-330.
27. Schmidt PC, Rubensdörfer CJW. (1994). Evaluation of Ludipress as a "multipurpose excipient" for direct compression: Part I: Powder characteristics and tableting properties. *Drug Dev Ind Pharm*, 20:2899-2925.
28. Casalderrey M, Souto C, Concheiro A, Gómez-Amoza JL, Martínez-Pacheco R. (2004). A comparison of drug loading capacity of cellactose with two ad hoc processed lactose-cellulose direct compression excipients. *Chem Pharm Bull*, 52:398-401.
29. Clerch AV. (2008). Aportacion al diseno de un nuevo excipiente tipo "co-processed product" para compresion directa. Barcelona: Universidad de Barcelona, 1-235.
30. Mužíková J, Nováková P. (2007). A study of the properties of compacts from silicified microcrystalline celluloses. *Drug Dev Ind Pharm*, 33:775-781.
31. BASF. (2007). Soluble Kollidon grades. *Tech Inf.*, Retrieved May 25, 2010, Available from [http://www.pharmaingredients.basf.com/Kollidon/TheKollidonProductFamily.aspx?WT.srch=1&WT.mc\\_id=Google%20Adwords&WT.seg\\_1=kollidon](http://www.pharmaingredients.basf.com/Kollidon/TheKollidonProductFamily.aspx?WT.srch=1&WT.mc_id=Google%20Adwords&WT.seg_1=kollidon). 1-16.
32. Baykara T, Duman G, Ozsener, KS, Ordu S, Ozates B. (1991). Comparing the compressibility of Ludipress with the other direct tableting agents by using acetaminophen as an active ingredient. *Drug Dev Ind Pharm*, 17:2359-2371.
33. Gohel MC, Parikh RK, Brahmabhatt BK, Shah AR. (2007). Preparation and assessment of novel co-processed superdisintegrant consisting of crospovidone and sodium starch glycolate: A technical note. *AAPS Pharm Sci Tech*, 8:63-69.
34. Hauschild K, Picker KM. (2004). Evaluation of a new co-processed compound based on lactose and maize starch for tablet formulation. *AAPS J*, 6:27-38.
35. Dressler JA, Wagner KG, Wahl MA, Schmidt PC. (2001). Comparison of incremental and inductive displacement transducers on an eccentric tablet press. *Phar Ind*, 63:886-893.
36. Bolhuis GK, Armstrong NA. (2006). Excipients for direct compaction—an update. *Pharm Dev Technol*, 11:111-124.
37. Fu Y, Pai CM, Park SY, Seomoon G, Park K. Inventors. (2004). Highly plastic granules for making fast melting tablets. EP1620075.
38. Jeong S, Kimura S, Fu Y, Park K. Inventors. (2005). Fast melting tablets having taste-masking and sustained release properties. WO/2006/101536.
39. Patel RP, Bhavsar MM. (2009). Directly compressible materials via co-processing. *Int. J Pharm Tech Res*, 1:745-753.
40. Gulian F, Simon B, Kurt A, LaBella G, Farrell T., Colorcon W. (2006). Evaluation of Star cap 1500® in a propranolol hydrochloride capsule formulation. Colorcon Retrieved May 27, 2010, Available from [http://www.colorcon.com/literature/marketing/ex/StarCap%201500/Pex\\_poster\\_starcap\\_prophcl\\_ver1\\_1105.pdf](http://www.colorcon.com/literature/marketing/ex/StarCap%201500/Pex_poster_starcap_prophcl_ver1_1105.pdf). pdf. 1105:1-5.
41. Mužíková J, Eimerová I. (2011). A study of the compaction process and the properties of tablets made of a new co-processed starch excipient. *Drug Dev Ind Pharm*, 37:576-582.
42. Legen I, Beso A, Reven S. Inventors. (2007). Pharmaceutical composition comprising hydrochlorothiazide and telmisartan. WO/2007/144175.
43. El-Barghouthi M, Eftaiha A, Rashid I, Al-Remawi M, Badwan A. (2008). A novel superdisintegrating agent made from physically modified chitosan with silicon dioxide. *Drug Dev Ind Pharm*, 34:373-383.
44. Auguello M, Ruzskay TA, Reier GE, Inventors. (1998). Co-processed microcrystalline cellulose and calcium carbonate. EP 0942950.
45. Auguello M, Ruzskay TA, Reier GE, Inventors. (1998). Co-processed products. US 5747067.
46. Gupta P, Nachaegari SK, Bansal AK. (2006). Improved excipient functionality by coprocessing. In: *Excipient Development for Pharmaceutical, Biotechnology and Drug Delivery Systems*. New York, USA: Informa Healthcare USA Inc. pp. 109-127.
47. Saigal N, Baboota S, Ahuja A, Ali J. (2009). Microcrystalline cellulose as a versatile excipient in drug research. *J Young Pharm*, 1:1-6.
48. Inghelbrecht S, Remon JP. (1998). Roller compaction and tableting of microcrystalline cellulose/drug mixtures. *Int J Pharm*, 161:215-224.
49. Carlin B. (2008). Direct compression and the role of filler-binders. In: *Pharmaceutical Dosage Forms: Tablets, Volume 2: Rational Design and Formulation*. Augsburg AL and Hoag SW, ed. 3rd ed. New York, USA: Informa Healthcare. pp. 173-216.
50. Thoores G, Leclercq B, Carlin B, Riley P, Garcia M, It P. inventors. (2008). Dry granulation binders, products, and use thereof. WO/2008/057266.
51. Garcia J, Ghaly ES. (2001). Evaluation of bioadhesive glipizide spheres and compacts from spheres prepared by extruder/marumerizer technique. *Pharm Dev Technol*, 6:407-417.
52. Battista O, Inventor. (1966). Shaped particles containing cellulose crystallite aggregates having an average level-off. US 3357845.
53. Battista O. (1965). Colloidal macromolecular phenomena. *J Polym Sci Polym Sym*, 9:135-155.
54. Mihranyan A, Edsman K, Strømme M. (2007). Rheological properties of cellulose hydrogels prepared from Cladophora cellulose powder. *Food Hydrocoll*, 21:267-272.
55. Bolhuis GK, Chowhan ZT. (1996). Materials for direct compression. In: *Pharmaceutical Powder Compaction Technology*. Alderborn G and Nystrom C, editors. New York: Dekker, pp. 419-500.
56. Lahdenpaa E, Antikainen O, Yliruusi J. (2001). Direct compression with silicified and non-silicified microcrystalline cellulose: Study of some properties of powders and tablets. *STP Pharma Sci*, 11:129-135.
57. Sherwood BE, Staniforth JH, Hunter EA. Inventors. (2004). Pharmaceutical excipient having improved compressibility. US 5,725,883.
58. van Veen B, Bolhuis GK, Wu YS, Zuurman K, Frijlink HW. (2005). Compaction mechanism and tablet strength of unlubricated and lubricated (silicified) microcrystalline cellulose. *Eur J Pharm Biopharm*, 59:133-138.

59. Gohel MC, Jogani PD, Bariya SE. (2003). Development of agglomerated directly compressible diluent consisting of brittle and ductile materials. *Pharm Dev Technol*, 8:143-151.
60. Sherwood B, Zeleznik JA, Schaible D, Berkulin W, Theissing K. Inventors. (2002). Agglomerated particles including an active agent co-processed with silicified microcrystalline cellulose. EP 1509204.
61. Kachrimanis K, Nikolakakis I, Malamataris S. (2003). Tensile strength and disintegration of tableted silicified microcrystalline cellulose: Influences of interparticle bonding. *J Pharm Sci*, 92:1489-1501.
62. Aljaberi A, Chatterji A, Shah NH, Sandhu HK. (2009). Functional performance of silicified microcrystalline cellulose versus microcrystalline cellulose: A case study. *Drug Dev Ind Pharm*, 35:1066-1071.
63. Zeleznik JA, Renak J. (2005). High functionality excipients (HFE)-Prosolv SMCC as an effective strategy for generic drug formulation. JRS Pharma L.P. Business Briefing: PharmaGenerics. pp 1-4
64. Limwong V, Sutanthavibul N, Kulvanich P. (2004). Spherical composite particles of rice starch and microcrystalline cellulose: A new co-processed excipient for direct compression. *AAPS PharmSciTech*, 5:e30.
65. Parrott EL. (1989). Comparative evaluation of a new direct compression excipient, Soludex™ 15. *Drug Dev Ind Pharm*, 15:561-583.
66. Celik M, Okutgen E. (1993). Excipient functionality. *Drug Dev Ind Pharm*, 19:2309-2334.
67. Olmo IG, Ghaly ES. (1999). Compressional characterization of two dextrose-based directly compressible excipients using an instrumented tablet press. *Pharm Dev Technol*, 4:221-231.
68. Kruse S, Gebert S, Kolter K. (2007). LudiFlash®-Easy and reliable development of orally dispersible tablets. *Exc Act*, 19:1-4.
69. Yidan L. (2008). A new excipient for fast disintegrating oral dosage forms. BASFp. 1 Retrieved August 10, 2010, Available from <http://www.phexcom.cn/UploadFiles/200899112624826.pdf>
70. SPI Pharma. (2007). Compressol ®S: Co-processed polyol. Technical Bulletin T135:1-2. Retrieved May 25, 2008, Available from [http://www.spipharma.com/downloads/Products/Excipients/Compressol\\_S/CompressolSTech.pdf](http://www.spipharma.com/downloads/Products/Excipients/Compressol_S/CompressolSTech.pdf)
71. Lieberman H, Lachman L, Schwartz J, Herbert, A., ed. (1989). *Pharmaceutical dosage forms: Tablets*. 2nd ed. New York: Marcel Dekker, pp. 225-232.
72. Abu-Taleb A, Aly S. (1985). Comparative evaluation of certain excipients and their binary blends for direct compression oxytetracycline hydrochloride tablets. *Drug Dev Ind Pharm*, 11:1971-1987.
73. El Sabbagh HM, El Shaboury MH. (1984). The use of directly compressible vehicles for the preparation of vitamin B1 tablets. *Pharmazie*, 39:237-239.
74. Es-Saheb, M. (1996). Tensile fracture characteristics of double convex-faced cylindrical powder compacts. *J. Mater Sci*, 31:214-223.
75. Shangraw R. (2002). Direct compression tableting. In: *Encyclopedia of Pharmaceutical Technology*. Swarbrick J and Boylan JC, ed. New York: Marcel Dekker. pp. 85-107.
76. Stout P, Howard S, Mouger J. (1991). Dissolution of pharmaceutical suspensions. In: *Encyclopedia of Pharmaceutical Technology*. Swarbrick J and Boylan J, ed. New York, USA: Marcel Dekker. pp. 169-192.
77. Ho R, Bagster DF, Crooks M. (1977). Flow studies on directly compressible tablet vehicles. *Drug Dev Ind Pharm*, 3:475-487.
78. Bowe K. (1998). Recent advances in sugar-based excipients. *Pharm Sci Technol Today*, 1:166-173.
79. Hurtt M, Pitkänen I, Knuutinen J. (2004). Melting behaviour of D-sucrose, D-glucose and D-fructose. *Carbohydr Res*, 339:2267-2273.
80. Morris LE, Moore JC, Schwartz JB. (1996). Characterization and performance of a new direct compression excipient for chewable tablets: Xylitab®. *Drug Dev Ind Pharm*, 22:925-932.
81. Ndindayino F, Henrist D, Kiekens F, Vervae C, Remon JP. (1999). Characterization and evaluation of isomalt performance in direct compression. *Int J Pharm*, 189:113-124.
82. Muziková J, Balhárková J. (2008). A study of the properties of tablets made of directly compressible maltose. *Ceska Slov Farm*, 57:21-27.
83. F-Melt® a new directly compressible excipient for fast oral disintegration tablets. Fuji Chemical industry Co.; c2009, Retrieved June 15, 2010, Available from [http://www.fujichemical.co.jp/english/newsletter/newsletter\\_pharma\\_0803.html](http://www.fujichemical.co.jp/english/newsletter/newsletter_pharma_0803.html)
84. Piene J. Inventor. (2005). Prebiotic combination products. EP1696937.
85. Rashid I, Al-Remawi M, Eftaiha A, Badwan A. (2008). Chitin-silicon dioxide co-precipitate as a novel superdisintegrant. *J Pharm Sci*, 97:4955-4969.
86. Teng Y, Qiu Z, Wen H. (2009). Systematical approach of formulation and process development using roller compaction. *Eur J Pharm Biopharm*, 73:219-229.
87. Cucala EJ, Siles OA, Gallego LM, It P. Inventors. (2006). Modified calcium phosphate excipient. US 7364755.
88. Baichwal AR, Staniforth JN, Inventors. (2000). Direct compressible sustained release excipient. US 6039980.
89. Baichwal AR, Staniforth JN, Inventors. (1992). Controlled release verapamil tablets. US 5169639.
90. McCall TW, Baichwal AR, Staniforth JN. (2003). TIMERx oral controlled-release drug delivery system. Rathbone M, Hadgraph J, Roberts M, ed. New York: Marcel Dekker, pp. 11-19.
91. Tobyn MJ, Staniforth JN, Baichwal AR, McCall TW. (1996). Prediction of physical properties of a novel polysaccharide controlled release system. I. *Int J Pharm*, 128:113-122.
92. Tobyn MJ, Maher J, Challinor CL, Staniforth JN. (1996). Investigations of the interactions between a novel polysaccharide controlled release matrix and model compounds using ESR. *J Control Rel*, 40:147-155.
93. Baichwal A, McCall TW, Inventors. (1995). Once a day metoprolol oral dosage form. US 5399362.
94. Kumar V, de la Luz Reus-Medina M, Yang D. (2002). Preparation, characterization, and tableting properties of a new cellulose-based pharmaceutical aid. *Int J Pharm*, 235:129-140.
95. Reus M, Lenz M, Kumar V, Leuenberger H. (2004). Comparative evaluation of mechanical properties of UICEL and commercial microcrystalline and powdered celluloses. *J Pharm Pharmacol*, 56:951-958.
96. de la Luz Reus Medina M, Kumar V. (2006). Evaluation of cellulose II powders as a potential multifunctional excipient in tablet formulations. *Int J Pharm*, 322:31-35.
97. de la Luz Reus Medina M, Kumar V. (2007). Modified cellulose II powder: Preparation, characterization, and tableting properties. *J Pharm Sci*, 96:408-420.
98. Rojas J, Kumar V. (2011). Comparative evaluation of silicified microcrystalline cellulose II as a direct compression vehicle. *Int J Pharm*, 416:120-128.
99. Rojas J, Kumar V. (2011). Coprocessing of cellulose II with amorphous silicon dioxide: Effect of silicification on the powder and tableting properties. *Drug Dev Ind Pharm*, DOI: 10.3109/03639045.2011.597400. 1-18.